

**TITLE: ACID SOLUBLE, HIGH FLUID LOSS PILL FOR
LOST CIRCULATION**

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Field of the Invention

The present invention relates to lost circulation materials (LCM), and to
10 spotting pills containing the LCM. More particularly, the invention relates to acid
soluble LCM's, and to spotting pills containing the LCM, preferably to spotting pills
having effective rheology and density.

Background of the Invention

15 Drilling fluids serve various functions, such as promoting borehole stability,
removing drilled cuttings from the wellbore, cooling and lubricating the bit and the
drillstring, as well as controlling subsurface pressure. Certain subsurface permeable
formations can cause, or lead to, "lost circulation," or the loss of whole drilling fluid
in quantity to the formation. In such a case, drilling of the well must be stopped and
20 the condition corrected. Examples of such subsurface permeable formations include,
but are not necessarily limited to: (1) natural or intrinsic fractures, (2) induced or
created fractures; (3) cavernous formations (crevices and channels), and (4)
unconsolidated or highly permeable formations (loose gravels).

Lost circulation materials (LCMs), or formation sealing agents, are used to
25 minimize the loss of drilling fluids into subsurface permeable formations by sealing
the formation. To prevent blow-out, or the uncontrolled flow of fluids from the
formation into the well, a "pill" or slug of the LCM is needed which has a density that
is similar to that of the drilling fluid used to treat the formation.

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In some cases the formations desired to be sealed may be a potential producing zone for hydrocarbons. Unfortunately, if the sealed formation is a producing formation, it may be difficult to subsequently produce hydrocarbons from the damaged zone. LCM's are needed which permit removal of the seal and allow for full recovery of hydrocarbons from the loss zone.

Summary of the Invention

The present application provides a high fluid loss spotting pill comprising: a carrier fluid; an LCM consisting essentially of an amount and form of acid soluble mineral particulate; said amount and said form being adapted to form a substantially impermeable, acid soluble filtercake upon injection of said composition with said carrier fluid into said wellbore and defluidization. In a preferred embodiment, the high fluid loss spotting pill preferably further comprises a weighting agent and a suspending agent effective to suspend said weighting agent. The quantity of weighting agent preferably is adapted to produce a density substantially the same as the density of a drilling fluid used to drill a formation being treated.

Detailed Description of the Invention

The present invention provides a high fluid loss squeeze type LCM pill for severe fluid losses for use in reservoirs and in general borehole applications. The pill is acid soluble for reservoir applications. The invention provides a high fluid loss LCM; a spotting pill comprising the LCM; a method of weighting up the spotting pill; a weighted spotting pill; and, a fast and effective method of remediation of a reservoir treated by the spotting pill. The LCM is suitable for use in water and oil based applications.

The LCM comprises acid soluble mineral particulates, preferably soluble salts of alkaline earth metals, most preferably calcium. Preferred acid soluble mineral particulates are calcium carbonate, more preferably a combination of granular calcium carbonate, and flaked calcium carbonate. The particulates have various particle size

5 distributions, as defined in the following Table:

Particle Size Distribution Analyses, in micron ranges

Calcium Carbonate Particulate Type:	<u>D (v, 0.1)</u>	<u>D (v, 0.5)</u>	<u>D (v, 0.9)</u>
Fine particulate (based on WO.-30 fine)	1 – 10	25 – 35	90 – 120
Coarse particulate (based on W.O.-30 coarse)	10 – 20	155 – 175	300 – 400
Fine flake (based on SOLUFLAKE fine)	10 - 20	160 - 180	400 - 500

The spotting pill comprises the LCM and a carrier fluid, preferably in slurry form. The spotting pill is injected into the loss zone to form a substantially impermeable filtercake to seal pores or fractures in the loss zone. Once the filtercake is thoroughly set, and losses stopped, the filtercake can be later remediated by exposure to an acid wash which solubilizes at least a portion of the filter cake and allows a free flowing reservoir for hydrocarbon production. The lost circulation pill can be used in both producing and non-producing intervals of the wellbore.

15 The spotting pill also preferably comprises one or more “suspending agents” that are capable of viscosifying the pill. Preferred suspending agents for use in water based slurries or “pills” are non-toxic and include, but are not necessarily limited to clays, water soluble starches and modified versions thereof, water soluble polysaccharides and modified versions thereof, water soluble celluloses and modified versions thereof, and water soluble polyacrylamides and copolymers thereof.

20 Preferred suspending agents for use in oil based slurries or “pills” also are non-toxic and include, but are not necessarily limited to organophilic clays, fatty acids, such as

dimer and trimer acids, and latex polymers. Generally, the quantity of suspending agent used is at least about 0.5 lb/bbl. or more, preferably about 2.0 lb/bbl. or more.

Clays that are suitable for use in water based slurries are not organophilic.

Clays that are suitable for use in oil-based slurries are organophilic, typically

5 quaternized clays. Suitable clays for either type of slurry or pill include, but are not necessarily limited to bentonite, montmorillonite, attapulgite, hectorite, sepiolite, and the like. A preferred clay for water based slurries is attapulgite. A preferred clay for oil based slurries is quaternized attapulgite. A most preferred suspending agent, and a preferred clay for use in both types of slurry is a ratio of about 50:50

10 attapulgite:quaternized attapulgite.

Starches that are suitable for use as suspending agents include, but are not necessarily limited to corn based and potato based starches, preferred starches being more temperature stable starches. Polysaccharides that are suitable for use as suspending agents include, but are not necessarily limited to xanthan polysaccharides,

15 wellan polysaccharides, scleroglucan polysaccharides, and guar polysaccharides.

Celluloses that are suitable for use as suspending agents include, but are not necessarily limited to hydrophobically modified hydroxyethyl celluloses and cationic cellulose ethers. Suitable copolymers of acrylamide include copolymers with acrylate monomers.

20 As used herein, the terms “modified starches” and “modified polysaccharides” or “synthetically modified polysaccharides” refer to starches and polysaccharides that have been modified in a manner that renders them inherently non-fermentable in order to avoid the need for a preservative. Water-soluble “modified starches” and “modified polysaccharides” that should operate successfully

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as water-soluble polymers include, but are not necessarily limited to: hydroxyalkyl
 starches and polysaccharides; starch and polysaccharide esters; cross-link starches and
 polysaccharides; hypochlorite oxidized starches and polysaccharides; starch and
 polysaccharide phosphate monoesters; cationic starches and polysaccharides; starch
 5 and polysaccharide xanthates; and, dialdehyde starches and polysaccharides. These
 derivatized starches and polysaccharides can be manufactured using known means,
 such as those set forth in detail in Chapter X of *Starch: Chemistry and Technology*
 311-388 (Roy L. Whistler, et al. eds., 1984), incorporated herein by reference.

Specific examples of suitable modified starches and modified polysaccharides
 10 include, but are not necessarily limited to: carboxymethyl starches and
 polysaccharides; hydroxyethyl starches and polysaccharides; hydroxypropyl starches
 and polysaccharides; hydroxybutyl starches and polysaccharides;
 carboxymethylhydroxyethyl starches and polysaccharides;
 carboxymethylhydroxypropyl starches and polysaccharides;
 15 carboxymethylhydroxybutyl starches and polysaccharides; epichlorohydrin starches
 and polysaccharides; alkylene glycol modified starches and polysaccharides; and,
 other starch and polysaccharide copolymers having similar characteristics.

The LCM

The LCM comprises a mixture of acid soluble components including but not
 20 necessarily limited to one or more acid soluble mineral particulates selected from the
 group consisting of granular and flaked mineral particulates. In a preferred
 embodiment, the acid soluble mineral particulates are a combination of granular
 calcium carbonate, and flaked calcium carbonate. By “acid soluble” is meant that an

unweighted filter cake formed by the LCM is about 85 wt.% or more acid soluble, preferably 90 wt.% or more acid soluble.

The acid soluble mineral particulate comprises substantially any acid soluble mineral, including but not necessarily limited to salts of alkaline earth metals, preferably carbonates of alkaline earth metals, silicates, hematites, and acid soluble mineral oxides, such as magnesium oxide, zinc oxide, calcium oxide, aluminum oxide, and the like. Preferred acid soluble mineral particulates are selected from the group consisting of carbonates and silicates, most preferably carbonates.

The acid soluble mineral particulate preferably has at least two particle sizes and/or forms. Preferably, the acid soluble mineral particulate is a combination of granular and flake form. The granular form comprises from about 0 to about 99 wt.%, preferably from about 25 to about 50 wt.%, more preferably about 50 wt.% of the LCM; the flake form comprises from about 0 to about 99 wt.%, preferably from about 25 to about 50 wt.%, more preferably about 25 wt.% of the LCM.

The granular acid soluble mineral particulates preferably have a "fine" particle size distribution. Suitable granular calcium carbonates are available from a variety of sources. A preferred granular calcium carbonate is WO-30 fine, available from Baker Hughes INTEQ.

The flaked acid soluble mineral particulates preferably have a "fine" particle size distribution, a preferred average diameter being from about 10 μm to about 400 μm . Suitable flaked acid soluble mineral particulates are available from a variety of commercial sources, and include, but are not necessarily limited calcium carbonate flake fine.

In a preferred embodiment, the acid soluble mineral particulate is calcium carbonate, preferably a combination of calcium carbonate in granular and flake form. A preferred embodiment of a blend without mineral fiber comprises from about 25 to about 50 wt%, preferably about 50 wt.% calcium carbonate flake fine and from about 25 to
 5 about 50 wt.%, preferably about 50 wt.% calcium carbonate fine.

A most preferred embodiment of a blend without mineral fiber has the following composition, as per a 100-lb. bag, and is suitable for both oil- and water-based systems:

10 45.3 lb Calcium Carbonate Flake fine
 45.3 lb Calcium Carbonate Particulate
 4.7 lb Saltwater gel
 4.7 lb quaternized attapulgite

The calcium carbonate particulate preferably is coarse. The saltwater gel aids in
 15 suspending the carbonate additives in the low-weight range of water-based slurries; quaternized attapulgite suspends the carbonate additives in oil-based slurries. Lime at 1 lb/bbl improves rapid filtration rates of the water-based slurries, particularly for the higher weight range (14 lb/gal and greater). For the oil-based formulations, it is preferred to use a wetting agent, such as OMNI-COTE®, at 0.5 – 1.0 lb/gal, when
 20 preparing the high density range fluids (16 – 18 lb/gal) to help wet the barite, thus making the slurries more pumpable. This LCM blend exhibited an acid solubility of 90.6%.

In another preferred embodiment, the LCM also comprises acid soluble mineral fiber. Mineral fibers are high purity mineral ores in fiber form that are
 25 available from a variety of commercial sources. Preferred acid soluble mineral fibers are extruded mineral wool, more preferably “fine” mineral wool. As used herein, the word “fine” means mineral fibers or wool having a diameter of from about 4 μ m to

about 20 μm , preferable from about 5 μm to about 6 μm , and a length of about 200 μm or less, preferably about 150 μm or less, more preferably from about 8 μm to about 25 μm . A most preferred embodiment comprising mineral fiber has the following composition:

- 5 at least about 10 wt.% mineral fiber, preferably about 25 wt.% fine mineral fiber;
- 10 from about 25 to about 50% granular acid soluble particulate, preferably fine particulate, preferably 50% granular acid soluble particulate fine, most preferably 50% calcium carbonate fine; and
- 15 from about 25 to about 50% acid soluble fine mineral flakes, preferably about 25 wt.% acid soluble mineral flake fine, most preferably about 25 wt.% calcium carbonate flake fine.

The acid soluble mineral particulates preferably have a particle size distribution effective to form a filter cake to block lost circulation of the drilling fluid to the formation, and to permit effective disintegration upon exposure to an acid wash. Depending upon the type of formation to be sealed, the acid soluble mineral

20 comprises particles ranging in mesh size from about 10 to about 25 mesh. In the foregoing preferred embodiment, the following weight percent of the LCM passes through screens having the following mesh sizes:

	10	5	% to	10	%
	14	5	% to	10	%
25	18	1	% to	5	%
	20	1	% to	5	%
	25	1	% to	5	%
	>25	87	% to	65	%

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The Spotting Pill

A high fluid loss rate is desirable so that when the slurry is placed within the zone of loss, the fluid rapidly enters the surrounding formation, thereby depositing a substantially impermeable filtercake or seal. In general, the higher the fluid loss rate, the thicker the filtercake in a given length of time, the more effective the LCM slurry. Fluid loss preferably is as high as possible while maintaining other properties in the desired ranges. As used herein, the term “high fluid loss” is defined to mean that defluidization occurs in 3 minutes or less, preferably 2 minutes or less, using a standard API fluid loss test (100 psi differential), and the following parameters:

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The resulting filtercake can have any hardness effective to seal the formation. Preferably, the filtercake has a hardness measured by a durometer, such as a PTC

Instruments, Model No. 411, of 30 or more, more preferably 40 or more, most preferably 50 or more.

The LCM may be premixed with the carrier fluid to form a slurry, mixed on site in slugging pits, or transferred by cement pumps. A sufficient amount of the LCM is added to the carrier fluid to form a slurry having substantially the same density as the drilling mud or drilling fluid being used. Conventional additives may be used as long as they do not interfere with the function or disintegration of the filtercake.

To prevent blow-out, or the uncontrolled flow of fluids from the formation into the well, the drilling fluid must have a density effective to provide a greater pressure than that exerted by the formation fluids. However, the density must not be carried too high, because excessive hydrostatic pressures can cause loss of circulation. Weighting materials frequently are added to increase the density of drilling fluids. A weighting material, such as ground barite, hematite, illmentie, iron carbonate (acid soluble), calcium carbonate (soluble), soluble salts, preferably salts of alkaline earth metals, such as sodium chloride, sodium bromide, calcium chloride, calcium bromide, and the like, preferably is added to adjust the density of the slurry to a desired level. The slurry preferably has a density substantially the same as the formation being treated, which typically is at least 9 lb./gal., and preferably from about 10 to about 18 lb./gal. The slurry generally comprises from about zero to about 600 pounds of barite per slurry.

Where the active, circulating system is weighted with barite or another weighting agent, the pill or slurry preferably is weighted up to substantially the same density in order to prevent pill migration as it is pumped and placed downhole. The

normal procedure is to use a reserve, slugging, or other inactive mud pit to mix the pill composition using either water or oil as the makeup fluid depending on whether the active system is a water based or an oil/synthetic based system. A portable tank/mixer or a cement unit also can be used to mix these high fluid loss LCM pills.

- 5 The weighting agent is added in either sack or bulk form usually through a hopper or, in the case of a high shear mixer, directly to the LCM pill composition, until the desired pill density is reached. Normal weighted pills will range in density from 8.4 to 21 lbs/gal. Normal volume will range from 30 to 200 barrels depending on the hole size being drilled and the extent of the suspected loss zone.

- 10 The resulting slurry has an effective plastic viscosity (PV) and yield point (YP). Generally, the yield point (YP) is above a minimum value to adequately suspend the LCM, the weighting materials, for example, barite and the like, if any are present, and any other components used in LCM fluids. Suspending agents are used to increase the yield point of the fluid without unduly increasing its viscosity.
- 15 Suspending agents preferably act to suspend or prevent settling out of the particulate matter without unduly increasing plastic viscosity or unduly decreasing fluid loss rates. Generally, the yield point for weighted systems is at least about 5 or more, preferably about 8 or more. Materials with yield point values below this minimum value have insufficient suspending ability to adequately suspend the LCM's,
- 20 weighting materials, and the like. For unweighted systems, it is preferred that the yield point be from about 5 to about 10 or less, preferably from about 1 to about 5 or less to facilitate pumping.

Spotting a slug of the LCM adjacent to the permeable formation is accomplished by methods known in the art. The "thief" or permeable formation

usually is at or near the bottom of the wellbore because, when the permeable formation is encountered, drilling fluid immediately is lost to the formation. In such situations the LCM fluid is spotted adjacent to the permeable formation by pumping a slug of the slurry down and out of the drill pipe. If the permeable formation is at a point farther up in the well bore, the drill pipe can be raised so that the slug of the LCM fluid is deposited adjacent the permeable formation.

The location of the loss zone is determined as accurately as possible. The bottom of the drill pipe or bit is placed at a depth that will allow an equivalent of the calculated open-hole volume to remain inside the casing above the casing shoe. The volume of the slug of slurry which is spotted adjacent the permeable formation can range from less than that of the open hole to more than double that of the open hole. The full open hole volume, plus additional barrels are pumped, leaving the remainder of the slurry in the casing. A sufficient quantity of the slurry is added to cover approximately 200% excess of the loss zone. Typically, from about 40 to about 100 bbl of the slurry is added. The spotting pill is pumped at from about 2 to about 10 bbls/min (bpm) with a rig pump until the pill reaches the loss zone at the end of the pipe. At this point the HYDRIL can be closed and a small amount of pressure from 200-400 psi can be applied to the pill to help facilitate movement of the pill to the loss zone and to defluidize the pill to form the LCM plug.

Defluidizing can be accomplished either by hydrostatic pressure or by exerting a low squeeze pressure. Hydrostatic pressure will complete the seal; however, low squeeze pressure is highly desirable because hydrostatic pressure may open incipient fractures or other areas of high permeability. Pumping begins again at from about 1 to about 2 bpm. When a pressure of about 500 psi is obtained, pumping is

discontinued for about 20 to about 60 minutes. The procedure is repeated until the required stabilized pressure is reached, at which point the LCM pill has been “defluidized.” A stabilized pressure maximum of about 500 to 800 psi is preferred.

Once a maximum holding pressure is achieved, the pressure is bled from the annulus and the filtercake is allowed to set for a period ranging from about 2 to 6 hours, preferably from about 3 to 8 hours, more preferably from about 4 to 8 hours. The filtercake produced by the foregoing procedures is effective to seal the formation, and may be herein referred to as a “substantially impermeable” filtercake.

Once set, the substantially impermeable filtercake is remediated by exposure to an acid wash to disintegrate the filtercake. A solution of acid is simply pumped down the well at a flow rate and for a period of time effective to dissolve at least a portion of the acid soluble minerals in the filtercake, thereby causing the filtercake to disintegrate. Preferably, the acid wash disintegrates the filtercake, which is sloughed or washed away. In a preferred embodiment, at least about 85 wt.% of the filtercake is removed by the acid wash, preferably at least about 90 wt.%. Where the LCM contains particulates only, and no mineral fiber, a preferred acid wash comprises an inorganic acid. Suitable inorganic acids include, but are not necessarily limited to hydrochloric acid, hydrobromic acid, nitric acid, chloric acid, sulfuric acid, hydrofluoric acid. The acid may have any concentration as long as it is sufficient to disintegrate the filtercake under the conditions of use. In a preferred embodiment, the acid wash has an acid concentration of from about 5 to about 36%. A preferred inorganic acid is hydrochloric acid at from about 5 to about 36%, preferably from about 5 to about 25%, most preferably about 10%.

Where the LCM contains particulates and mineral fiber, a preferred acid wash comprises both an inorganic acid and an organic acid at a ratio and concentration, respectively, effective to disintegrate the filtercake and convert silicon oxide in the mineral fiber to soluble silicic acid. Substantially any water soluble organic acid may be used in combination with the inorganic acid to treat the mineral fiber. Suitable organic acids include, but are not necessarily limited to acetic acid and citric acid. A preferred acid wash when mineral fibers are present is a 60/40 blend of the inorganic acid and the organic acid, respectively. A preferred organic acid for use in this blend is acetic acid at from about 1 to about 5%, preferably about 3%.

The invention will be better understood with reference to the following Examples, which are illustrative only.

Experimental blends

The following experimental blends were tested in the following Examples.

The fractions refer to a 2 gram sample:

- 15 **Blend #1**
Mineral Fiber Fine 1/3
Calcium Carbonate Flake Fine 1/3
Calcium Carbonate Fine Particulate 1/3
- 20 **Blend #2**
Mineral Fiber Fine 1/2
Calcium Carbonate Flake Fine 1/4
Calcium Carbonate Fine Particulate 1/4
- 25 **Blend #3**
Mineral Fiber Fine 1/4
Calcium Carbonate Flake Fine 1/4
Calcium Carbonate Fine Particulate 1/2
- 30 **Blend #4**
Mineral Fiber Fine 1/4
Calcium Carbonate Flake Fine 1/2
Calcium Carbonate Fine Particulate 1/4

Example 2

Particle size distributions were determined for the experimental blends by sonic sifting. Two grams of each blend was sifted for 15 minutes under the following conditions:

ATM Sonic Sifter Analysis

Sample	2 grams
Sift time	15 minutes
Amplitude	1
Mode	Sift/Pulse

The results were as follows:

Blend #1

Mineral Fiber Fine 1/3

Calcium Carbonate Flake Fine 1/3

Calcium Carbonate Fine Particulate 1/3

Screen Mesh Number	Initial Weight	Final Weight	Difference	Weight % Through
10	49.45	49.62	0.17	8.5%
14	48.09	48.27	0.18	9%
18	45.47	45.57	0.10	5%
20	44.72	44.74	0.02	1%
25	44.10	44.11	0.01	0.05%
Pan	157.13	158.60	1.47	73.5%

Blend #2

Mineral Fiber Fine 1/2

Calcium Carbonate Flake Fine 1/4

Calcium Carbonate Fine Particulate 1/4

Screen Mesh Number	Initial Weight	Final Weight	Difference	Weight % Through
10	49.45	49.60	0.15	7.5%
14	48.09	48.29	0.20	10%
18	45.47	45.57	0.10	5%
20	44.72	44.75	0.03	1.5%
25	44.10	44.13	0.03	1.5%
Pan	157.13	158.67	1.54	77%

Blend #3

Mineral Fiber Fine 1/4

Calcium Carbonate Flake Fine 1/4

- 5 Calcium Carbonate Fine Particulate 1/2

Screen Mesh Number	Initial Weight	Final Weight	Difference	Weight % Through
10	49.45	49.58	0.13	6.5%
14	48.09	48.22	0.13	6.5%
18	45.47	45.54	0.07	3.5%
20	44.72	44.73	0.01	0.05%
25	44.10	44.11	0.01	0.05%
Pan	157.13	158.71	1.58	79%

Blend #4

- 10 Mineral Fiber Fine 1/4

Calcium Carbonate Flake Fine 1/2

Calcium Carbonate Fine Particulate 1/4

Screen Mesh Number	Initial Weight	Final Weight	Difference	Weight % Through
10	49.45	49.48	0.03	1.5%
14	48.09	48.18	0.09	4.5%
18	45.47	45.49	0.02	1%
20	44.72	44.73	0.01	0.5%
25	44.10	44.12	0.02	1%
Pan	157.13	158.93	1.80	90%

Competitive product A

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Screen Mesh Number	Initial Weight	Final Weight	Difference	Weight % Through
10	49.45	49.61	0.16	8%
14	48.09	48.26	0.17	8.5%
18	45.47	45.68	0.21	10.5%
20	44.72	44.84	0.12	6%
25	44.10	44.20	0.10	5%
Pan	157.13	158.37	1.24	62%

Example 3

A standard API fluid loss test (100 psi differential) , was performed on the four experimental blends described in Examples 1-2 and compared to two other commercially available products using the following parameters:

30 lb/bbl system
Whatman 541 filter paper
100 psi.

The carrier fluid was water. In weighted slurries, the amount of water used was sufficient to give 350 ml of finished product. After the product had been added to the water, stirring of the resulting slurry continued for 10 minutes at low shear of 1500 rpm. After stirring, the slurry was transferred to a standard API filter press cell containing the Whatman filter paper at the base. At a pressure of 100 psi, the time required for complete fluid loss was recorded. The results are shown below.

Product	Time (seconds)	Amount (ml)
Blend #1	16	162.09
Blend #2	13	160.12
Blend #3	13	164.91
Blend #4	12	162.06
Competitive Product A	13	162.24
Competitive Product B	24	157.61

The rate of complete fluid loss of Blend #4 was slightly lower than the other blends.

Example 4

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The procedures of Example 3 were repeated using a pressure of 50 psi, also measuring the hardness of the filtercake formed. The following are the results:

Product	Time (sec)	Amount (ml)	Filtercake Thickness (cm)	Filtercake Hardness	Comments
Blend #1	19	162.67	0.6	31	
Blend #2	17	160.7	0.6	33	
Blend #3	17	162.14	0.55	51	Has more calcium medium than other blends.
Blend #4	20	163.41	0.6	34	
Competitive Product A	19	159.46	0.7	15	Surface uneven.
Competitive Product B	33	155.68	0.65	59	

Blend #3 exhibited a relatively rapid fluid loss combined with a high durometer hardness filtercake.

The filtercakes formed by the experimental blends had two distinct layers.

- 5 The actual mineral fiber component of the blend was in the lower layer. These filtercakes seemed fragile. Two layers were also seen with the Competitive Product A and the filtercake was very fragile. Competitive Product B filtercake was indeed a rigid plug, as the literature suggests.

Example 5

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The procedures of Examples 2 and 3 were followed to form a filter cake, with the exception that no filter paper was used. A standard seawater drilling mud was prepared having the following composition:

Mud Formulation

Component	Concentration	Amount
Tapwater	1.0 bbl	3500 ml
Bentonite	10 ppb	100 g
NaCl	14 ppb	140 g
Chrome lignosulfonate	5 ppb	50 g
Lignite	3 ppb	30 g
Caustic soda	1 ppb	10 g
Soda Ash	1 ppb	10 g
PAC LV	0.5 ppb	5 g

One lab barrel of the mud was run through the filtercake formed above for 30 minutes at 100 psi. The fluid loss was recorded, as follows:

5	Results:	
	Blend #1	19.6 ml
	Blend #2	23.5 ml
	Blend #3	18.5 ml
	Blend #4	18.5 ml
10	Competitive Product A	53 ml
	Competitive Product B	30 ml

Blends #3 and #4, which contained 25% mineral fiber, exhibited the least fluid loss,

15 thus indicative of better sealing-off of further fluid invasion.

Example 6

Blend #3 slurries in either water or oil were weighted up with barite to produce slurries having from 10 to 18 lb/gal. The filtration rates were measured and filtercake properties noted. The weighted up slurries exhibited desirable high filtration rates. Filter cake depositions were good, comparable to those prepared with Competitive Product B. Minimal treatments with either saltwater gel (attapulgate, for water based fluids) or quaternized attapulgate (for oil based fluids) were necessary to help suspend Blend #3 in the low weight ranges. A surfactant or wetting agent was used at 1 lb/bbl to help wet the barite in the 18 lb/gal range; the same was true for

25 Competitive Product B.

The following Table give the water-based slurry formulations used:

Weight , lb/gal	10	12	14	16	18
Water, bbl	0.90	0.83	0.76	0.69	0.62
Saltwater gel, lb	3.0	3.0	3.0	2.0	1.0
Competitive Product B, lb	42.6	35.8	29.3	23.9	18.4
Barite, lb	60	180	290	400	520

Weight (ppg)	10	12	14	16	18
Water, bbl	0.90	0.83	0.76	0.69	0.62
Blend #3, lb	42.6	35.8	29.3	23.9	18.4
Barite, lb	60	180	290	400	520

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In order to weight up the water based slurries, water, lost circulation material, and barite were weighed out according to the following formulations tables. If used, the saltwater gel was added to water and mix for 10 minutes at 1500 rpm. The LCM was added and the resulting fluid was mixed for one minute at 2000rpm. Then, the barite was added and the resulting fluid was mixed for 5 minutes at 2000rpm. A higher shear of 3000rpm was used for the final mixing step of the 18 lb/gal slurries.

After mixing, the slurry was loaded into an API cell and the fluid loss test was run at 100 psi with no filter paper. The fluid amount was recorded at minute intervals until blowout, and then a final fluid loss was recorded at blowout. The fluid retained in the filtercake was calculated and recorded. Also, the filtercake thickness and hardness were recorded.

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slurries:

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Competitive Product B

Weight	Fluid Retained (mls)	Fluid Loss (mls)	Time	Filtercake Thickness	Filtercake Hardness
10 lb/gal	55	200 260	1 minute 1min 35 sec	1.9 cm	65
12 lb/gal	60.5	175 230	1 minute 1min 55 sec	2.5 cm	65
14 lb/gal	66	150 200	1 minute 2 min 7 sec	3.3 cm	60
16 lb/gal	61.5	125 175 180	1 minute 2 minutes 2 min 11 sec	3.8 cm	60
18 lb/gal	77	100 125 140	1 minute 2 minutes 2 min 18 sec	4.6 cm	40

The following Table give the oil-based slurry formulations used:

Density , lb/gal	10	12	14	16	18
Oil, bbl	0.876	0.805	0.735	0.666	0.596
(g)	261	240	219	198	177
Quaternized attapulgite, lb	3	2	1	1	-
Competitive Product B, lb	42.6	35.8	29.3	23.9	18.4
Barite, lb	115	230	342	454	564
Omni-Cote, lb	-	-	-	-	1.0

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Density	10	12	14	16	18
Oil, bbl	0.876	0.805	0.735	0.666	0.596
(g)	261	240	219	198	177
Quaternized attapulgite, lb	3	2	1	1	-
Blend #3	42.6	35.8	29.3	23.9	18.4
Barite, lb	115	230	342	454	564
Omni-Cote, lb	-	-	-	-	1.0

In order to weight up the oil based slurries, oil, lost circulation material, and barite were weighed out according to formulations tables. If used, quaternized attapulgite was added and mixed for 10 minutes at 1500rpm. The LCM was added and the fluid was mixed for one minute at 2000rpm. The barite was then added and the fluid was mixed for 5 minutes at 2000rpm. The slurry was then loaded into an API cell and the fluid loss test was run at 100 psi with no filter paper. The fluid amount was recorded at minute intervals until blowout, and then a final fluid loss was recorded at blowout. The fluid retained in the filtercake was calculated and recorded. Also filtercake thickness and hardness were recorded. The results are given in the following Tables:

Blend #3

Weight	Fluid Retained (mls)	Fluid Loss (mls)	Time	Filtercake Thickness	Filtercake Hardness
10ppg	26.3	80	1 minute	2.5 cm	5
		125	2 minutes		
		160	3 minutes		
		190	4 minutes		
		220	5 minutes		
		245	6 minutes		
		265	7 minutes		
		280	8 minutes		
		300	8 min 38 sec		
12ppg	25	75	1 minute	3.2 cm	10
		100	2 minutes		
		130	3 minutes		
		150	4 minutes		
		170	5 minutes		
		185	6 minutes		
		200	7 minutes		
		210	8 minutes		
		225	9 minutes		
		240	10 minutes		
		250	11 minutes		
		265	12 minutes		
		275	13 minutes		
14ppg	48.8	85	1 minute	3.6	<5
		125	2 minutes		
		145	3 minutes		
		170	4 minutes		
		185	5 minutes		
		200	6 minutes		
		220	7 minutes		
		225	7 min 35 sec		
16ppg	57.5	65	1 minute	4.0 cm	<5
		85	2 minutes		
		105	3 minutes		
		125	4 minutes		
		145	5 minutes		
		160	6 minutes		
		170	7 minutes		
		190	8 min 10 sec		
18ppg	41.3	50	1 minute	4.1	65
		60	2 minutes		
		70	3 minutes		
		75	4 minutes		

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		85	5 minutes		
		95	6 minutes		
		105	7 minutes		
		110	8 minutes		
		115	9 minutes		
		125	10 minutes		
		155	15 minutes		
		175	20 minutes		
		180	21 minutes		

*Test was mistakenly thought to be finished. But when the cell was opened up, there was still oil on top of the filtercake. Test was put back on and continued for another 15 minutes.

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Competitive Product B

Weight	Fluid Retained (mls)	Fluid Loss (mls)	Time	Filtercake Thickness	Filtercake Hardness
10ppg	31.3	120	1 minute	2.2 cm	25
		150	2 minutes		
		175	3 minutes		
		200	4 minutes		
		220	5 minutes		
		240	6 minutes		
		250	7 minutes		
		265	8 minutes		
		275	9 minutes		
		295	10 min 6 sec		
12ppg	52	100	1 minute	2.9cm	<5
		125	2 minutes		
		145	3 minutes		
		165	4 minutes		
		180	5 minutes		
		195	6 minutes		
		205	7 minutes		
		220	8 minutes		
		240	9 minutes		
		245	10 minutes		
		248	10 min 16 sec		
14ppg	68.8	70	1 minute	3.2	<5
		125	2 minutes		
		155	3 minutes		
		170	4 minutes		
		185	5 minutes		
		200	6 minutes		
		205	6 min 21 sec		

TABLE DEB-6660

16ppg	72.5	80 105 130 145 155 175	1 minute 2 minutes 3 minutes 4 minutes 5 minutes 5 min 55 sec	4.4 cm	<5
18ppg	71.3	20 50 75 85 100 125 135 140 148 150	1 minute 2 minutes 3 minutes 4 minutes 5 minutes 6 minutes 8 minutes 9 minutes 10 minutes 11 minutes	4.6	31

Filtercakes produced by Competitive Product B contracted at 14ppg and above. The contraction is believed to contribute to faster fluid loss times. The Blend #3 filter cakes have two layers, with the mineral fibers making up the lower part of the filtercake. Competitive Product B behaves in a similar manner, but the thickness of the filtercake seems to be the same among all the filtercakes.

Example 7

The acid solubility of Blend #3 was compared to that of Competitive Product B. 5 grams of Blend #3 was weighed out, mixed with a 60:40 blend of 10% hydrochloric acid and 3% acetic acid, respectively, and the mixture was heated to 170°F. The mixture was stirred with a magnetic stirrer and heated to 170°F for 45 minutes. Then, the mixture was filtered through a #42 Whatman filter paper (2.7 micron) using a Buchner funnel under vacuum. The residue was weighed and the percent acid solubility calculated.

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Persons of ordinary skill in the art will recognize that many modifications may be made to the present invention without departing from the spirit and scope of the present invention. The embodiment described herein is meant to be illustrative only

and should not be taken as limiting the invention, which is defined in the following claims.

[illegible]